

CO₂ Sequestration in Mining Residues – Probing Heat Effects Associated to Carbonation

By MSc student
Aksenova Diana

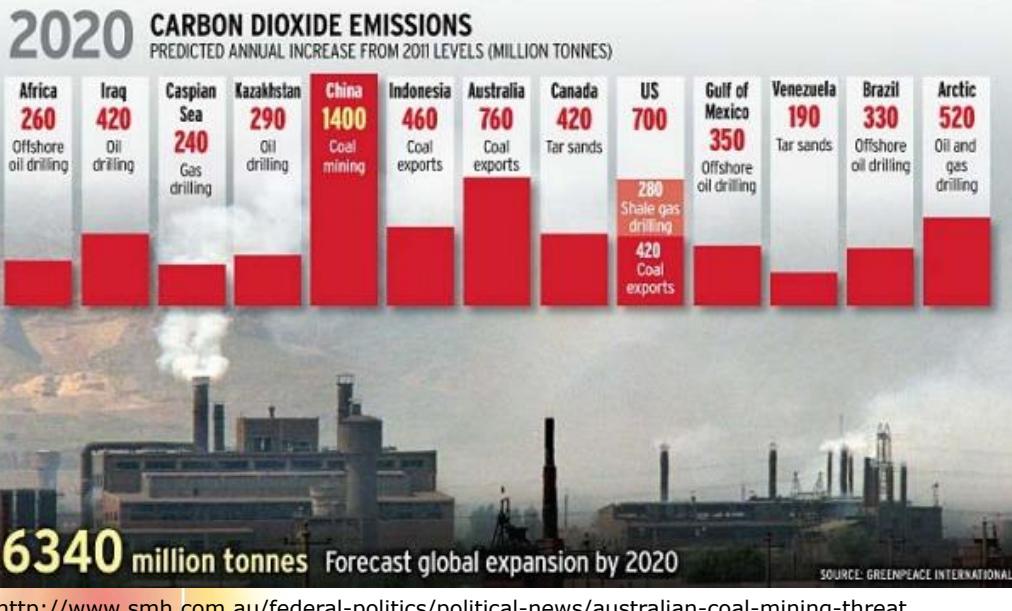
Department of Chemical Engineering

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Co-Supervisors: Prof. Xavier Maldaque
and Prof. Georges Beaudoin

Content

- Raison d'être du travail / Purpose of the project
- Bibliographie et problématique / Literature review
- Description du projet de thèse / Description of the project
- Méthodologie du projet proposé / Methodology
- Résultats préliminaires / First results
- Conclusion
- Échéancier envisagé / Education plan

Purpose of the project CO₂ emissions

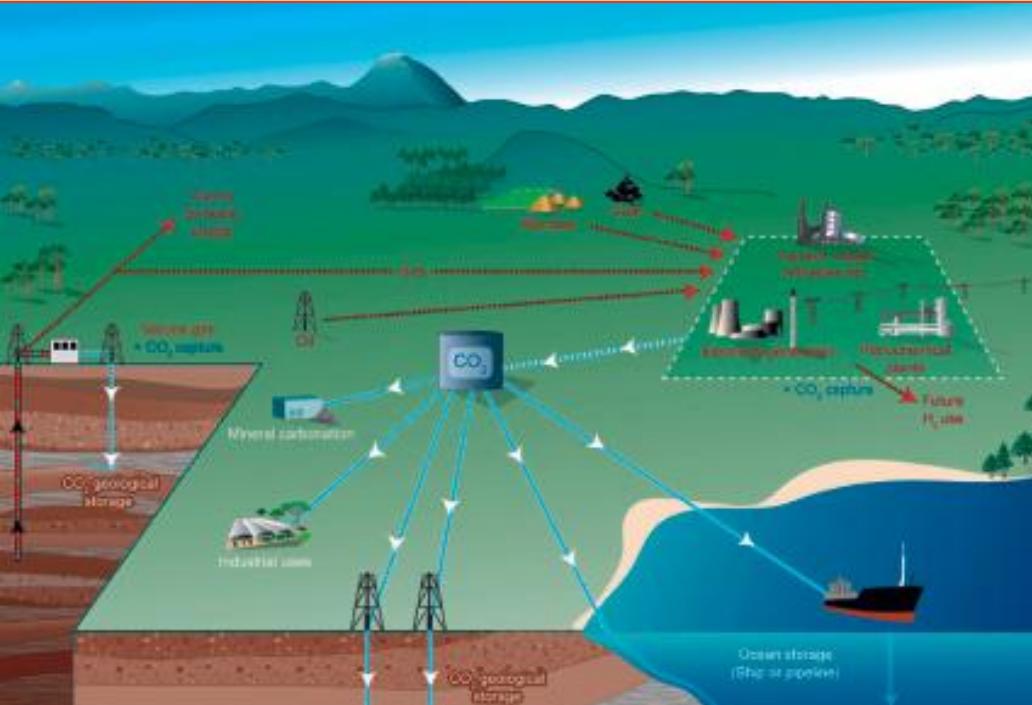


March, 2016 – 404,83 ppm

If CO₂ emissions continue to rise, the enhanced greenhouse effect may permanently change the climate system in the world.

According to the IPCC association, an increase in the global average surface temperature more than 2°C contains potential significant damage to the ecosystems upon which we depend directly.

Literature review CO₂ capture and storage



(IPCC Special Report on Carbon Dioxide Capture and Storage, p. 4)

Capture:

- Absorption (amines, carbonates, ammonia, hydroxide)
- Adsorption (metal organics, zeolites)
- Membranes (fibers, microporous)
- Biological (algae, cyanobacteria)

Storage:

- Geological
- Ocean
- **Mineral**

Mineral sequestration

- **W. Seifritz**, *CO₂ disposal by means of silicates* (1990)
- **H. Dunsmore**, *A geological perspective on global warming and the possibility of carbon dioxide removal as calcium carbonate mineral* (1992)
- **K. Lackner et al.**, *Carbon dioxide disposal in carbonate minerals* (1995)
- **O'Connor et al.**, *Carbon dioxide sequestration by direct mineral carbonation with carbonic acid* (2000)

Direct carbonation

Accomplished through the reaction of a solid alkaline mineral with CO₂ either in the gaseous or aqueous phase

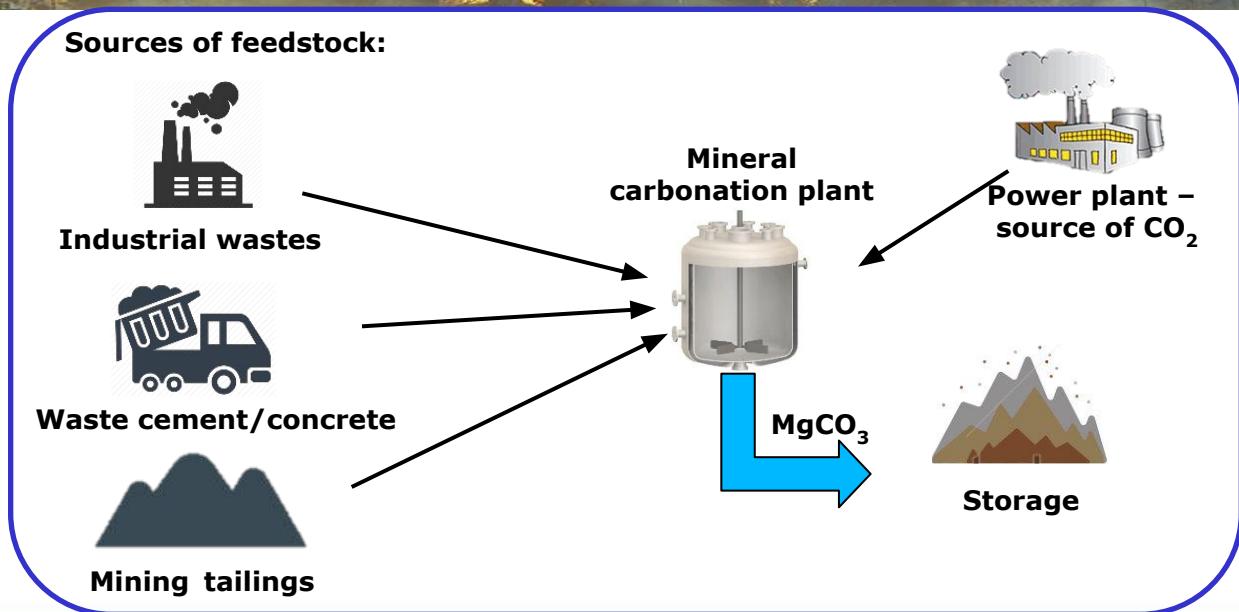
Indirect carbonation

Involves the extraction of reactive components (Mg²⁺, Ca²⁺) from the minerals, using acids or other solvents, followed by the reaction of the extracted components with CO₂ either in the gaseous or aqueous phase

Active carbonation concept



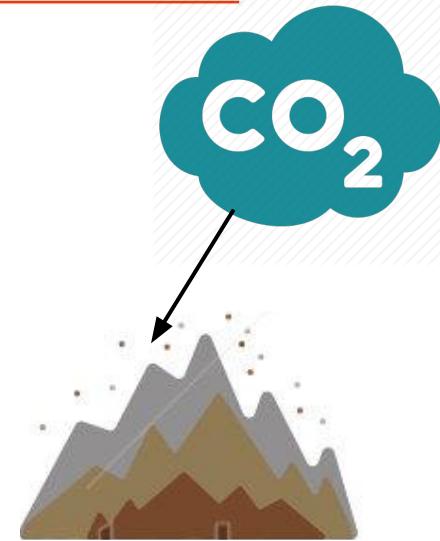
- The Netherlands
- Finland
- Japan
- China
- U.S. and Canada
- Switzerland
- Australia



Passive carbonation by tailings



- 1) Long term stability
- 2) Raw materials are abundant
- 3) Potential to be economically viable



- 1) Low speed of the process
- 2) No control under ambient conditions

ULaval group

- **G. Assima:**

- 1) The presence of the T difference in a reactor between bed with NiMR and recirculating gas
- 2) Water content accelerates the process and leads to the bigger CO₂ capture
- 3) More alkaline carbonates are formed at elevated temperatures

- **J. Pronost:**

- 1) Hot-spots in the waste heap surface – the sign of the exothermic behavior of the reaction
- 2) Carbonation potential of ultramafic material depends on the brucite content

- **A. Entezari Zarandi:**

- 1) The rapid CO₂ uptake in the early minutes of reaction caused a sharp drop in pH
- 2) The highest carbonation reactivity is attained with 3% brucite doping of an already carbonated NiMR
- 3) Carbonation proceeds through formation of a porous flaky carbonate phase topping mainly the high-pH brucite surfaces

Description of the project

Primary challenge



(http://cdn1.buuteeq.com/upload/15348/asbestos-mine-tailings-mountain-1.jpg.1140x481_default.jpg)

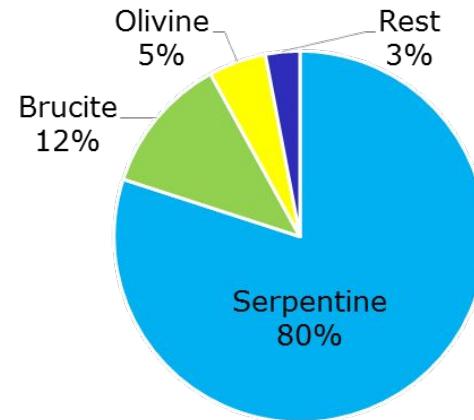
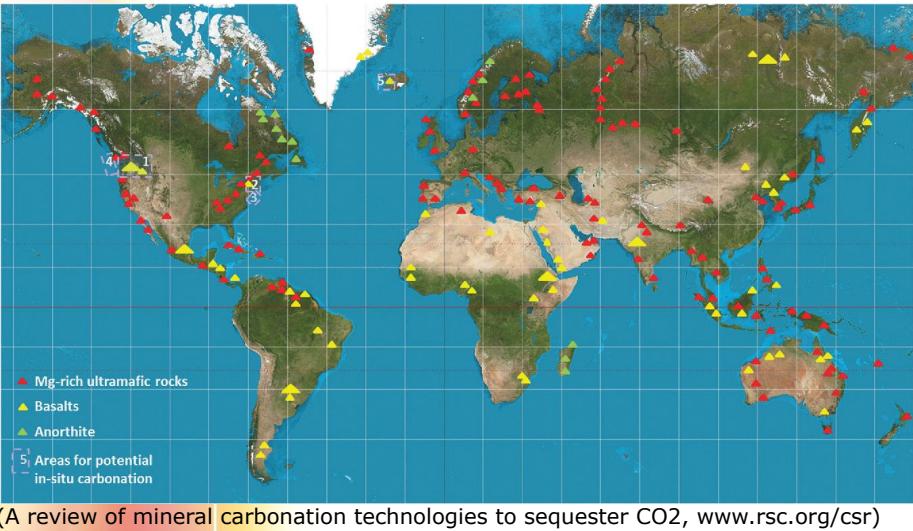
What's new?



- Deep investigation of the ore behavior under ambient conditions by using IR thermography
- The way to get back some energy and use it for an industrial needs

Mining tailings

Mafic and ultramafic residues are the best feedstock for the CO₂ sequestration.



- Serpentine group(Lizardite)~80-90%
- Brucite ~ 0-12%
- Olivine group (Forsterite) ~ 5%
- Rest ~ 3%

Group of minerals based on **Magnesium carbonate** is an environmentally stable and non-toxic.

Experimental procedure



(<https://nuclear-news.net/information/wastes/>)

Winter

- $T = -20 \dots 0^{\circ}\text{C}$
- $\text{H}_2\text{O sat.}(\text{snow}) = 50 \dots 100\%$

Spring/Autumn

- $T = 0 \dots +15^{\circ}\text{C}$
- $\text{H}_2\text{O sat.}(\text{rain}) = 50 \dots 100\%$

Summer

- $T = +15 \dots +30^{\circ}\text{C}$
- $\text{H}_2\text{O sat.}(\text{rain}) = 0 \dots 50\%$

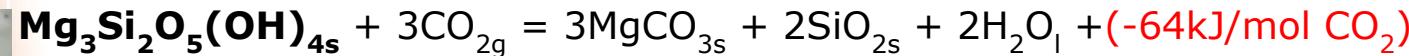
Theoretical & real carbonation reactions

Brucite



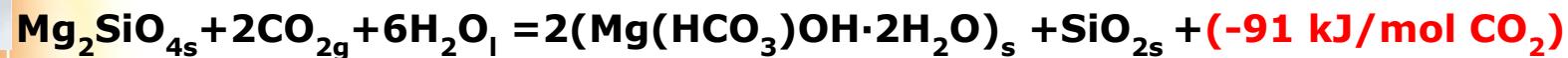
-1,95 MJ/kg of CO₂

Lizardite



-1,64 MJ/kg of CO₂

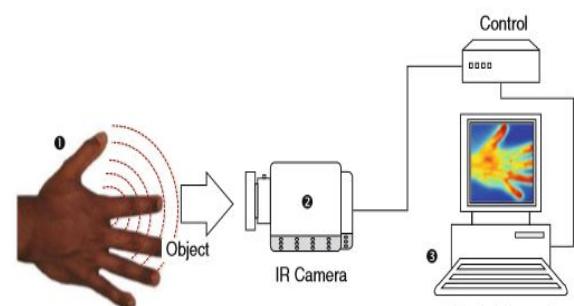
Forsterite



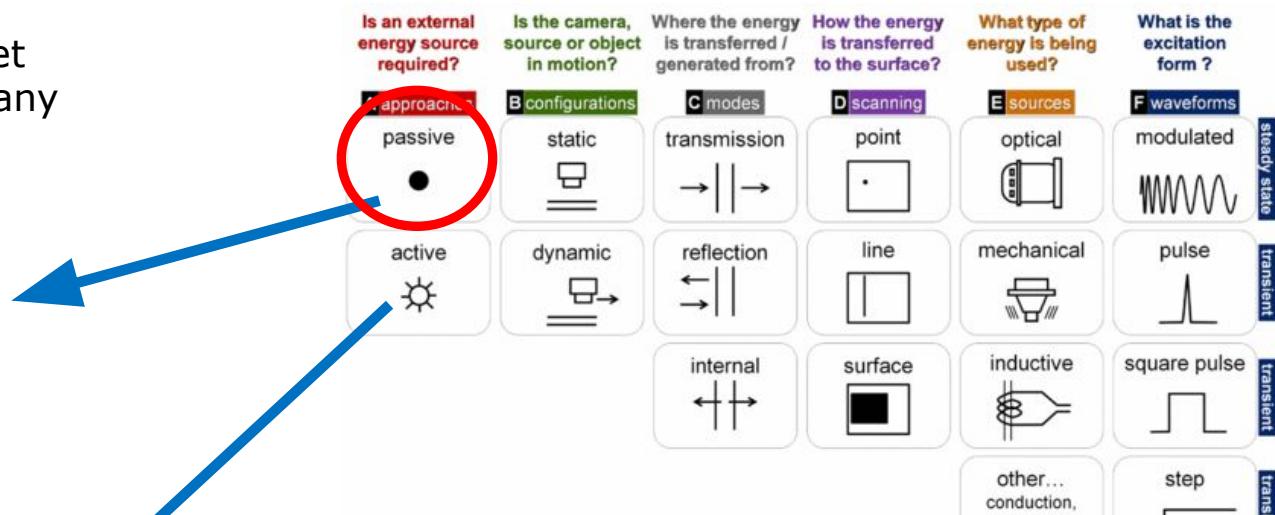
-2,07 MJ/kg of CO₂

Infrared thermography

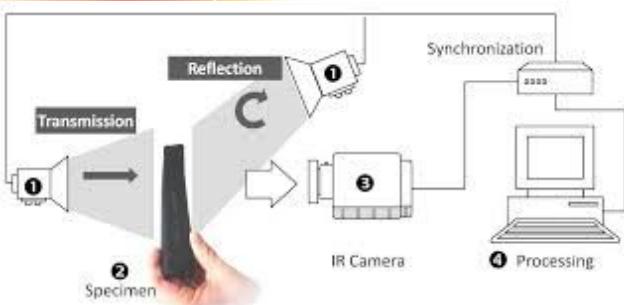
Radiation coming from the target object is measured without any external heat stimulation



(Infrared Thermography, C. Ibarra-Castanedo and X. P. V. Maldague, p. 178)



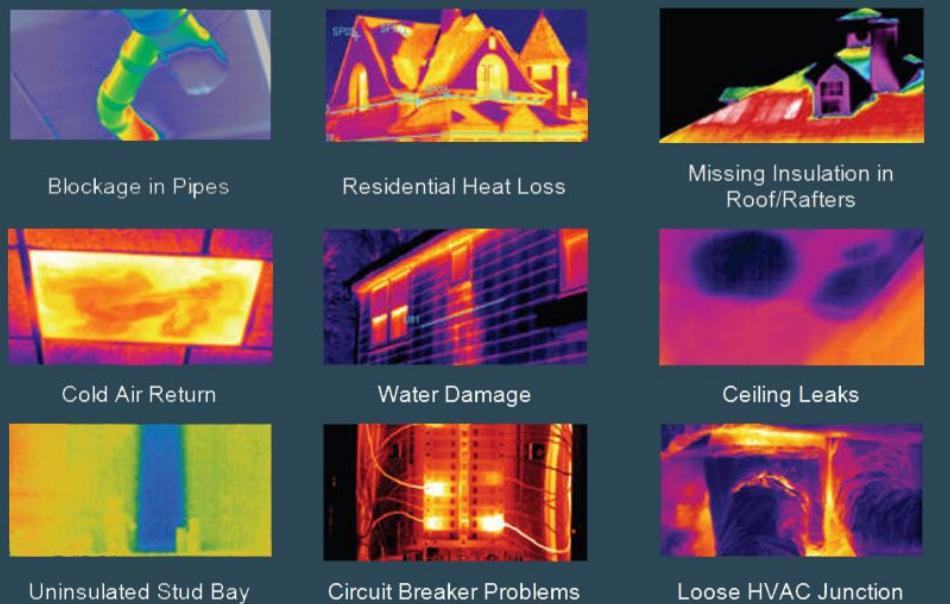
(Infrared Thermography, C. Ibarra-Castanedo and X. P. V. Maldague, p. 180)



(Infrared Thermography for NDT: Potentials and Applications, X. P. V. Maldague, slide 19)

Energy source is required to produce a thermal contrast between the feature of interest and the background

Infrared camera



(<http://fiveboroughhomeinspection.com/inspection-service/infrared-camera-inspection-service/>)

Thermal image data is colored up pixel by pixel based on $T^{\circ}\text{C}$.

Indigo Phoenix Thermal Camera

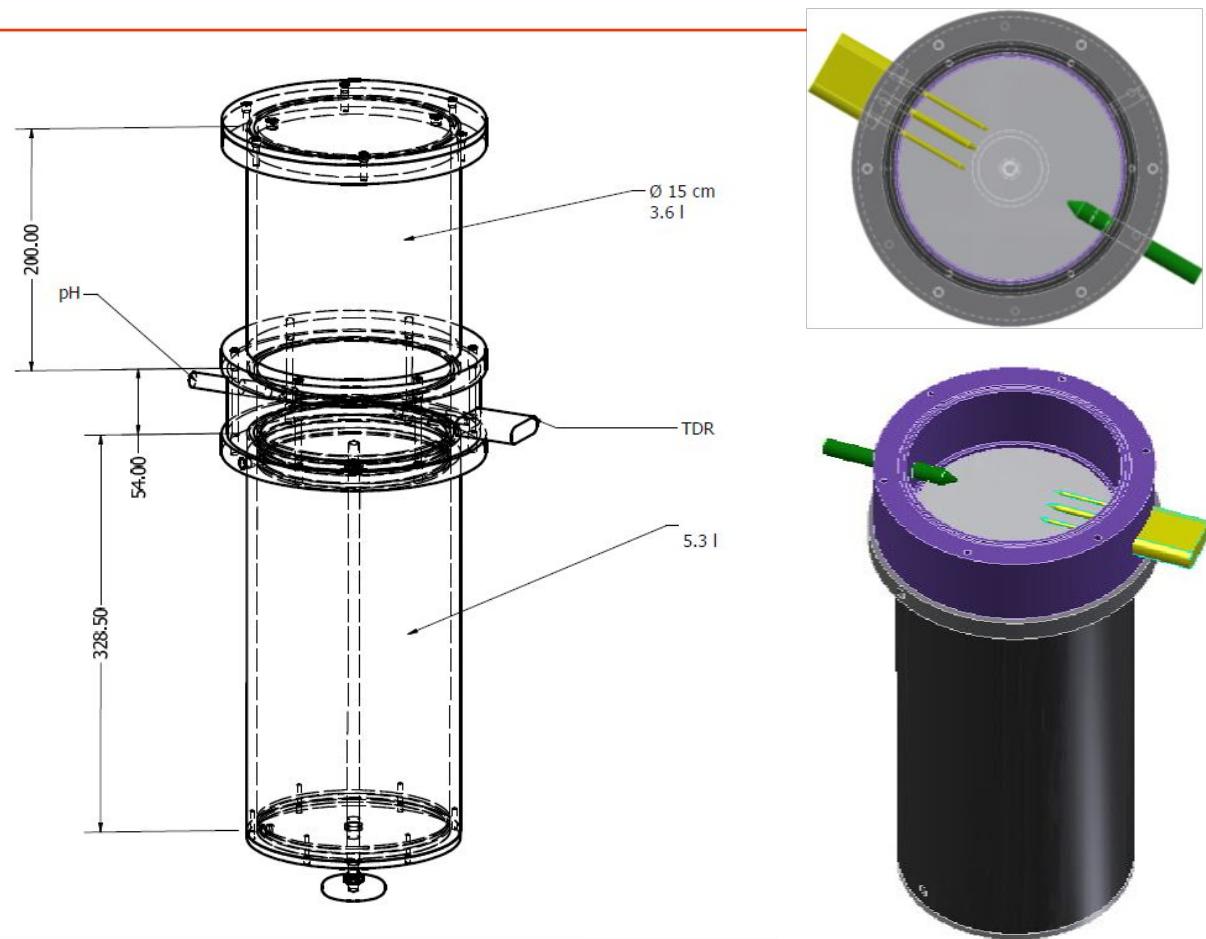
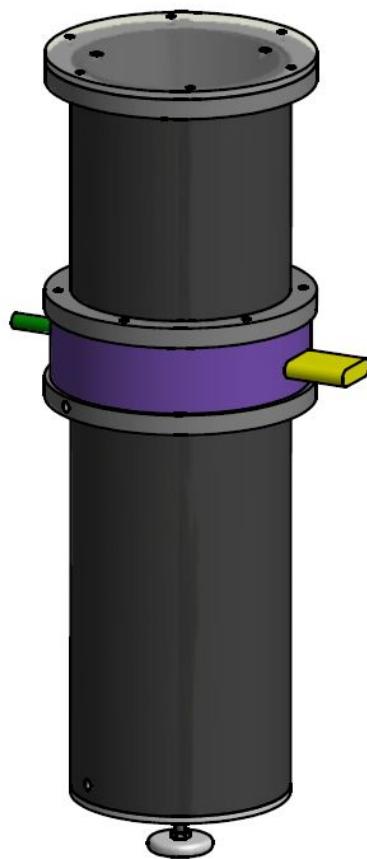


(<http://www.tiir.com/legacy/view/?id=51542>)

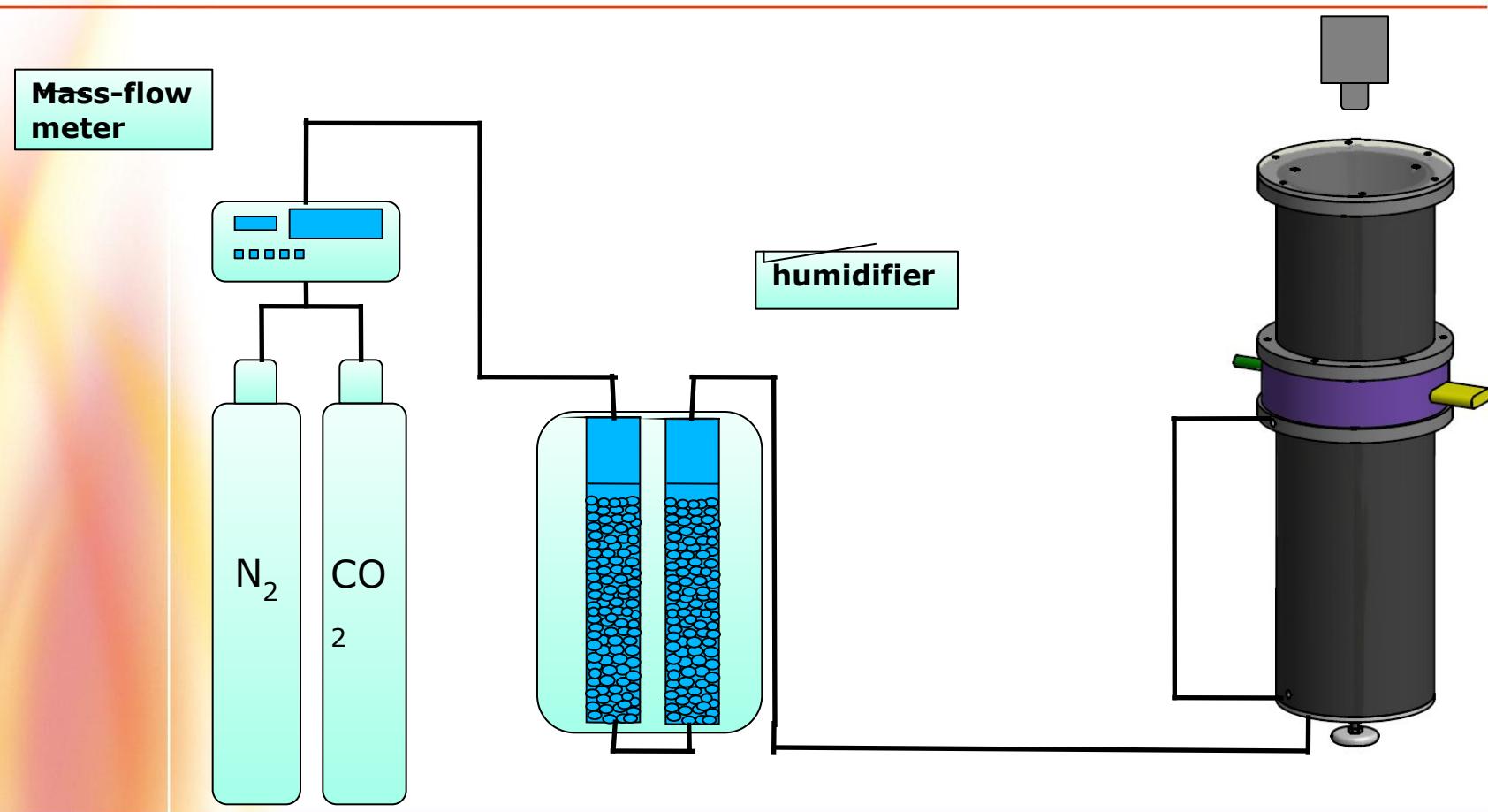


Methodology

Design of the setup



Carbonation setup



Chemistry of the laboratory process

50 g of ORE + 0,047 mol of CO₂ (1,06 l), 50% water saturation :

	CO ₂ , mol	Q, J	Cp(prod.), J/mol*K	ΔT, K
Mg(OH) _{2s} + CO _{2g} + 2H ₂ O _l = Mg(HCO ₃)OH · 2H ₂ O _s + (-86 kJ/mol)	0,0078	669,52	301,71	2,22
2Mg ₃ Si ₂ O ₅ (OH) _{4s} + 3CO _{2g} + 6H ₂ O _l = 3(Mg(HCO ₃)OH · 2H ₂ O) _s + Mg ₃ Si ₄ O ₁₀ (OH) _{2s} + (-72,4 kJ/mol)	0,0234	1492,79	1226,84	1,38
Mg ₂ SiO _{4s} + 2CO _{2g} + 6H ₂ O _l = 2(Mg(HCO ₃)OH · 2H ₂ O) _s + SiO ₂ + (-91 kJ/mol)	0,0156	1418,26	647,99	2,19

9 g of ore will react with 1,02 l of CO₂

Carbonation reaction with brucite



Laboratory conditions: $\omega(\text{CO}_2) = 20\%$, $T=298\text{K}$,
50% saturation

$$V_{\text{CO}_2} = 1,06 \text{ litres}$$

$$n(\text{CO}_2) = 0,047 \text{ mol}$$

$$\Delta_r H = -85836 \text{ J/mol of CO}_2$$

$$Q = -\Delta_r H \cdot n = 4061,88 \text{ J}$$

$$Q = C_p \cdot \Delta T$$

$$\Delta T = 13,46\text{K}$$

Ambient conditions(mine site): $\omega(\text{CO}_2) = 400\text{ppm}$, $T=298\text{K}$,
50% saturation

$$V_{\text{CO}_2} = 0,00212 \text{ litres}$$

$$n(\text{CO}_2) = 9,46 \cdot 10^{-5} \text{ mol}$$

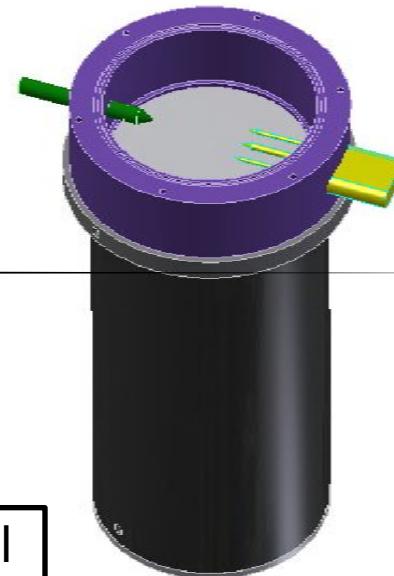
$$\Delta_r H = -85836 \text{ J/mol of CO}_2$$

$$Q = -\Delta_r H \cdot n = 8,12 \text{ J}$$

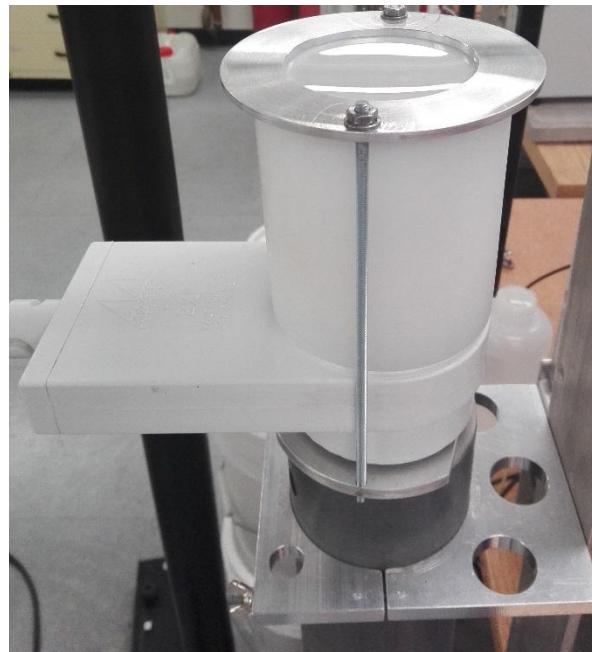
$$Q = C_p \cdot \Delta T$$

$$\Delta T = 0,027\text{K}$$

$$V_{\text{total}} = 5,3 \text{ l}$$



Reactor available in the laboratory of Prof. Larachi



Estimation for A. Entezari Zarandi setup

35 g of ore + 0,009 mol CO₂ (50% water saturation)

	CO ₂ , mol	Q, J	Cp(prod.), J/mol*K	ΔT, K
Mg(OH) _{2s} + CO _{2g} + 2H ₂ O _l = Mg(HCO ₃)OH · 2H ₂ O _s + (-86 kJ/mol)	0,0015	128,75	301,71	0,43
2Mg ₃ Si ₂ O ₅ (OH) _{4s} + 3CO _{2g} + 6H ₂ O _l = 3(Mg(HCO ₃)OH · 2H ₂ O) _s + Mg ₃ Si ₄ O ₁₀ (OH) _{2s} + (-72,4 kJ/mol)	0,0045	287,07	994,27	0,26
Mg ₂ SiO _{4s} + 2CO _{2g} + 6H ₂ O _l = 2(Mg(HCO ₃)OH · 2H ₂ O) _s + SiO ₂ + (-91 kJ/mol)	0,003	272,74	647,99	0,42

Carbonation reaction with Mg (OH)₂



Laboratory conditions: $\omega(\text{CO}_2) = 10\%$, $T = 298\text{K}$, 50% saturation

$$V_{\text{CO}_2} = 0,2 \text{ litres}$$

$$n(\text{CO}_2) = 0,009 \text{ mol}$$

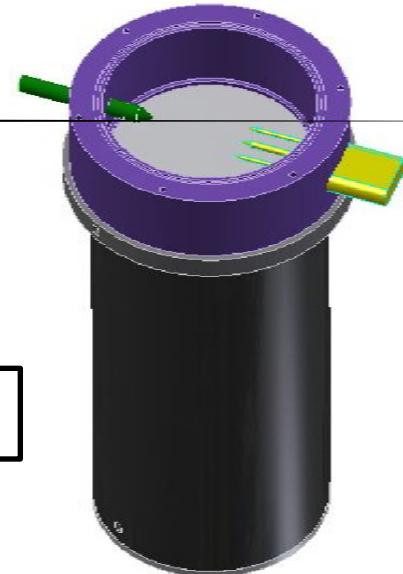
$$\Delta_r H = -94714 \text{ J/mol of CO}_2$$

$$Q = -\Delta_r H \cdot n = 766,39 \text{ J}$$

$$Q = C_p \cdot \Delta T$$

$$\Delta T = 2,54\text{K}$$

$$V_{\text{total}} = 2 \text{ l}$$



Summary table for brucite

% CO2	400ppm -ambient amount of CO2	20% - new setup	10%- Ali's setup
V (total), l	5,3	5,3	2
V (CO2), l	0,00212	1,06	0,2
Q, J	8,12	4061,88	766,39
ΔT, K	0,027	13,46	2,54

First results - Brucite

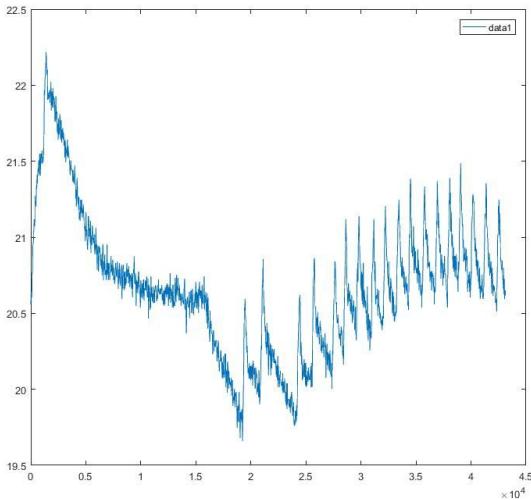
35g Mg(OH)₂ (11%) + SiO₂

- 5,25 ml of H₂O = 50% sat.
- 9.69% of CO₂
- Duration = 15 h
- 0.56% of CO₂ left

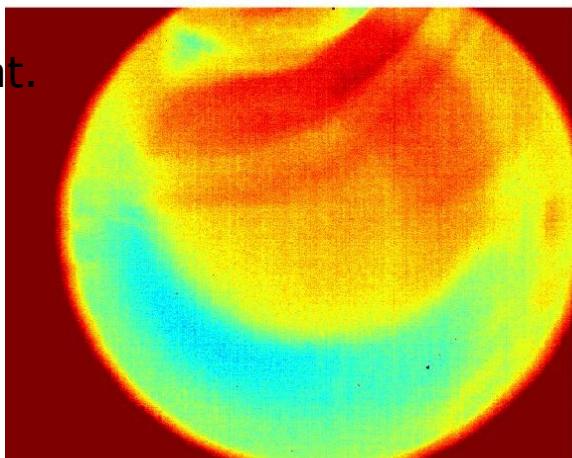
First results - ORE

35 g of the ore

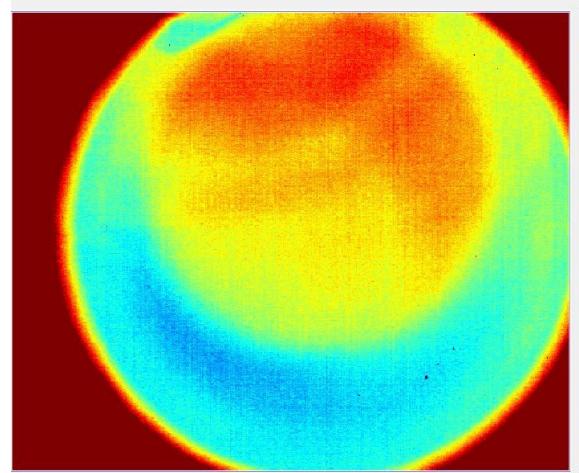
- 4,37 ml of H₂O = 50% sat.
- 9.83% of CO₂
- Duration = 9 h



15 min



30 min



33 min: T = 22.25 C, ΔT=1.65 C

Summary

- Investigate
- Get
- Utilize

Q



(http://cdn1.buuteeq.com/upload/15348/asbestos-mine-tailings-mountain-1.jpg.1140x481_default.jpg)

Education plan

	2016			2017
	Winter	Summer	Autumn	Winter
Literature search				
Experiments				
Courses	CHM- 6002		GCH-7011	GCH-6000 GIF-7006
Writing a thesis				

CHM-6002: Propriétés et réactivité des surfaces

GCH-7011: Planification et analyse des expériences

GCH-6000: Communication scientifiques orale et écrite I

GIF-7006: Vision en inspection industrielle

CO₂ Sequestration in Mining Residues – Probing Heat Effects Associated to Carbonation

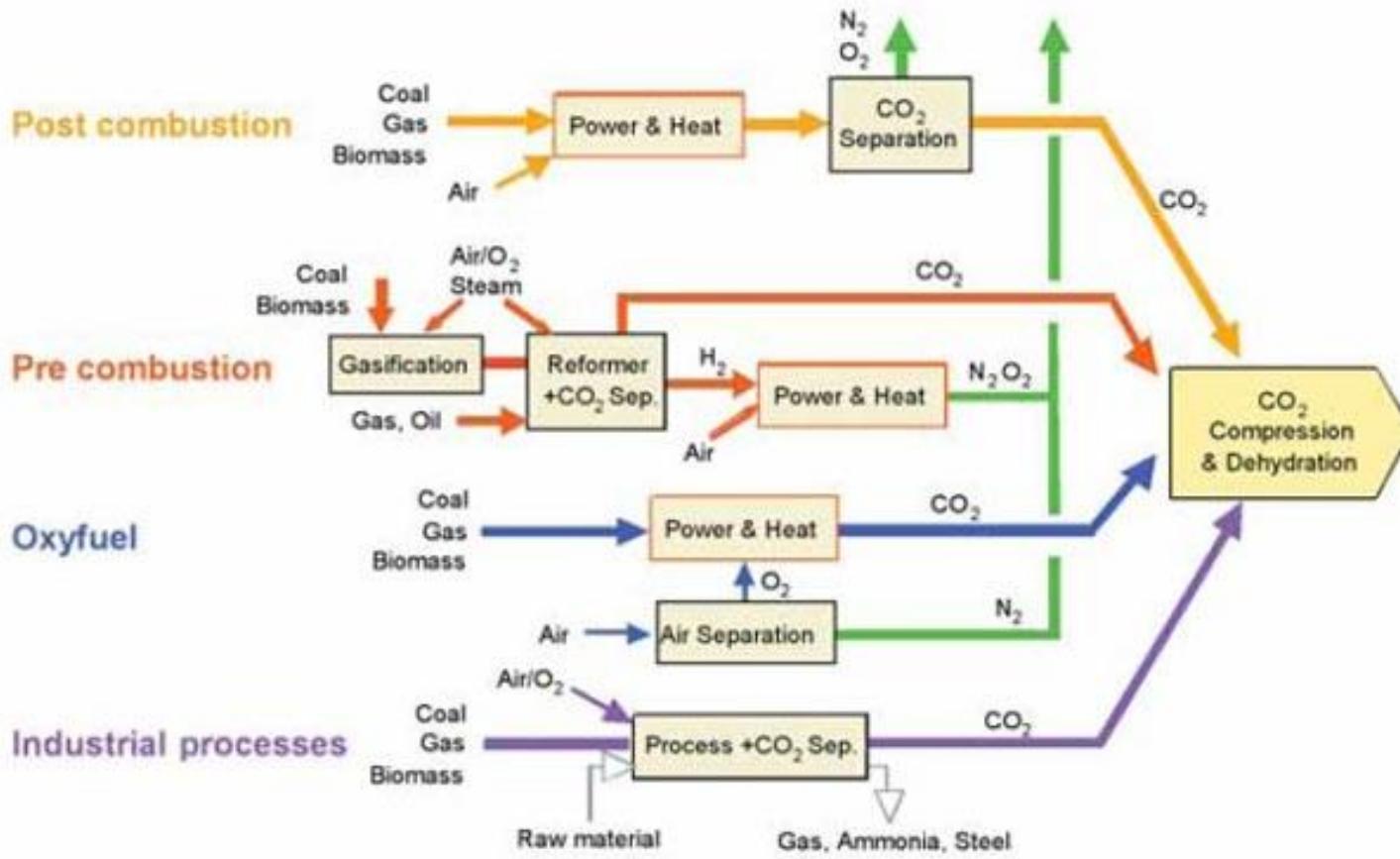
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Questions

CCS

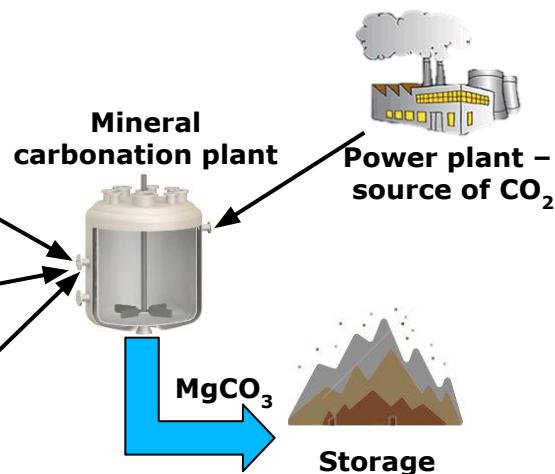


[Carbon Dioxide Capture and Storage: Technical Summary \(2005\)](#)

Active carbonation concept

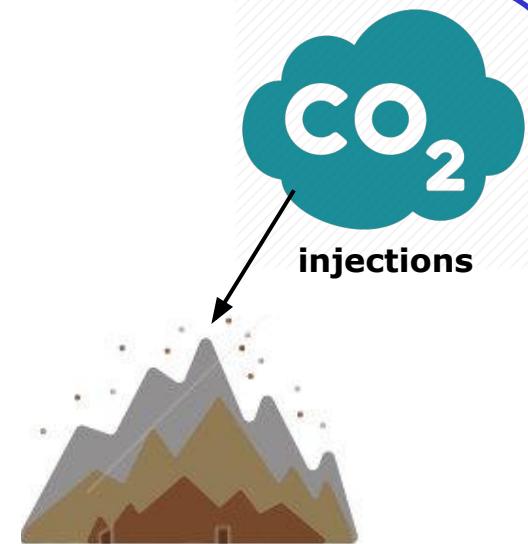
Ex-situ

Sources of feedstock:

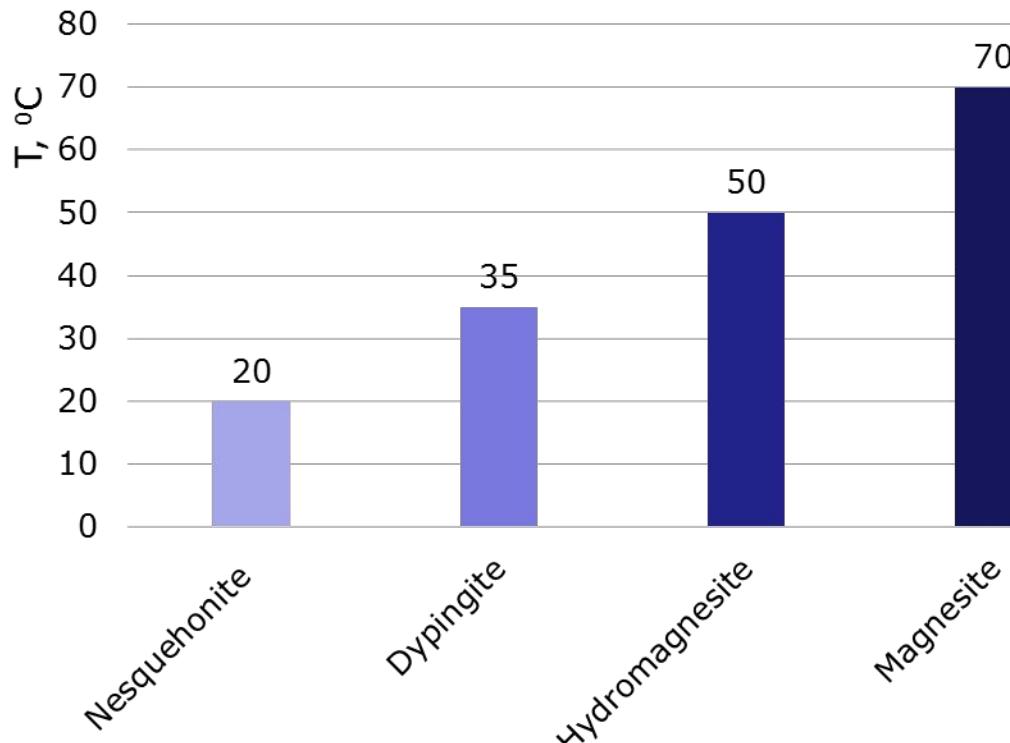
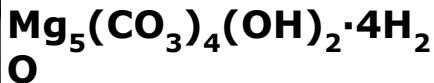
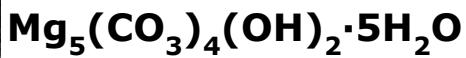


In-situ

OR

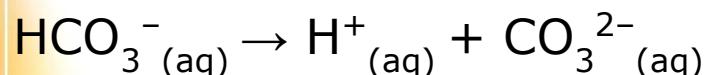
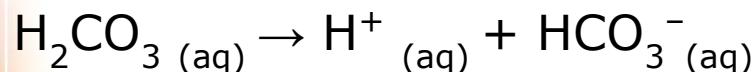
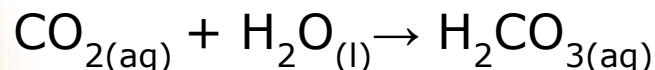
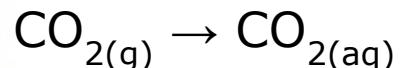


Reaction products of sequestration

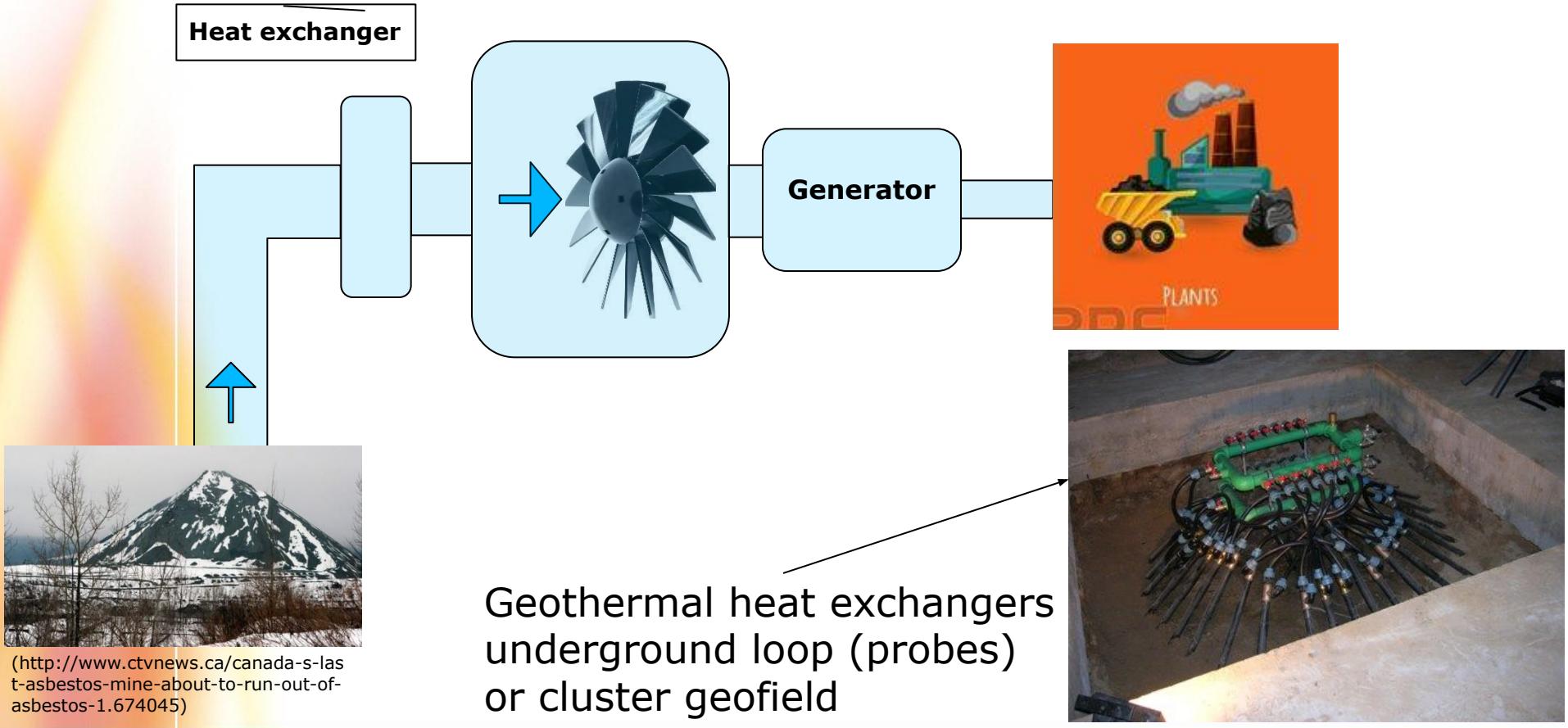


(<http://www.mindat.org/min-1979.html>)

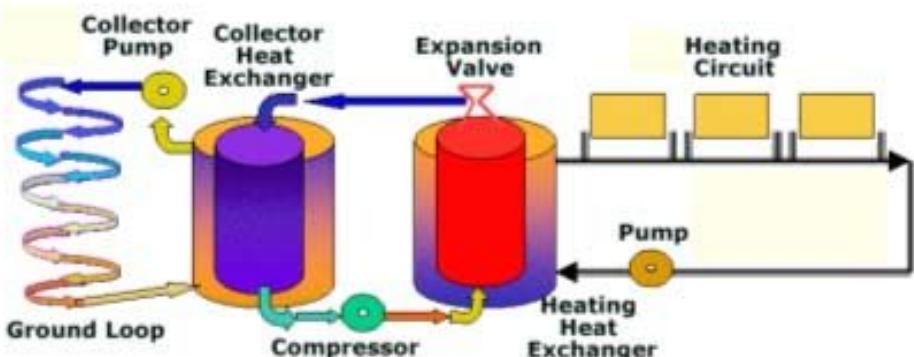
Mg²⁺ – series of the reactions



Future investigations



Future investigations

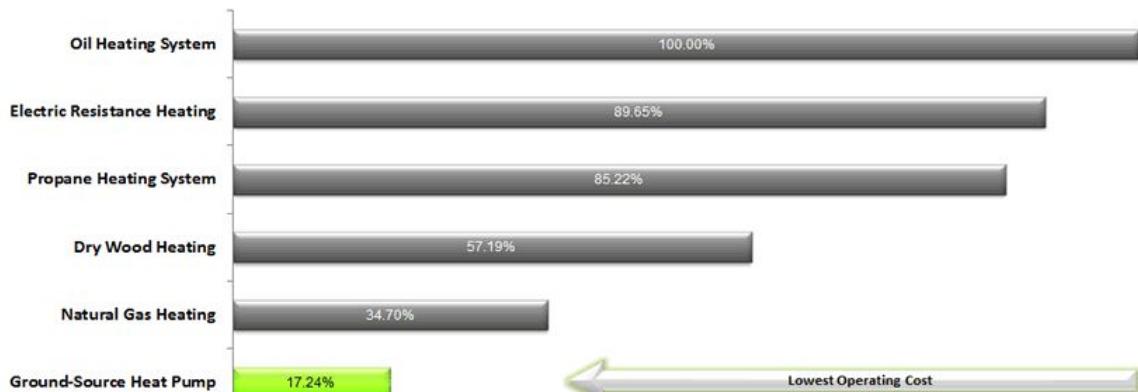


(<http://www.diydoctor.org.uk/green-living/green-living-projects/ground-source-heat-pumps.htm>)

Using the heat pump, 1 kW geothermal heat energy is converted into thermal energy in 4 kW and above, there is an energy consumption - 25%

Heating Costs Comparison

Estimates based on the following energy costs:
Electricity - \$0.09/ kWh; Oil - \$3.26 / gallon; Propane - \$1.95/ gallon; Dry Wood - \$210 / full cord; Natural Gas - \$0.98 / therm

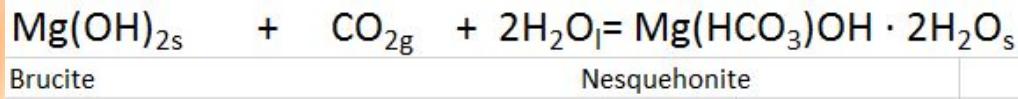


(<http://www.luxtherm.com/what-is-a-geothermal-heat-pump.html>)

Detailed calculations for Mg (OH)₂



Mg(OH)2:



$\omega(\text{CO}_2)$, %	0,04	20	10
V(total), l	5,3	5,3	2
V(CO ₂), l	0,00212	1,06	0,2
V _m , l/mol	22,4	22,4	22,4
n(CO ₂), mol	9,46429E-05	0,047	0,009
ΔrH , J/mol CO ₂	-85836	-85836	-85836
Q, J	8,12	4061,88	766,39
Cp(products), J/mol*K	301,71	301,71	301,71
ΔT , K	0,027	13,463	2,540

$$V(\text{CO}_2) = \frac{\omega \cdot V(\text{total})}{100\%}$$

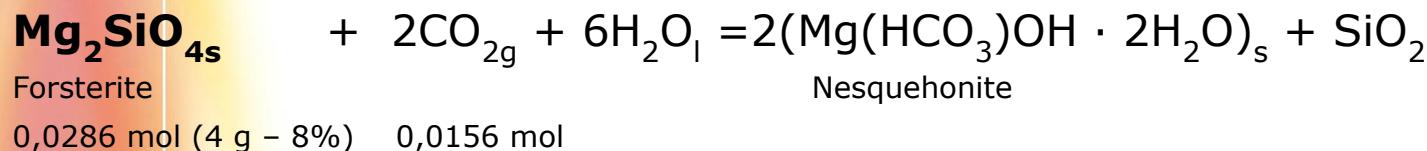
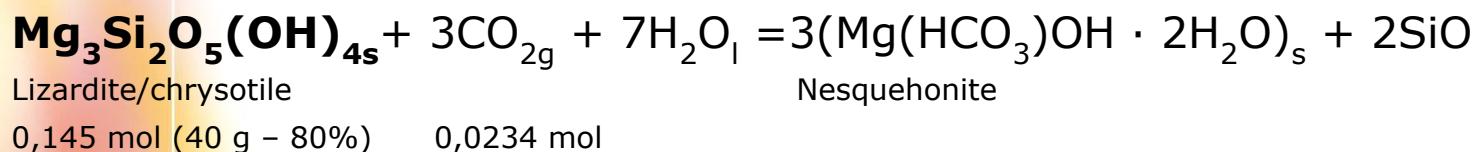
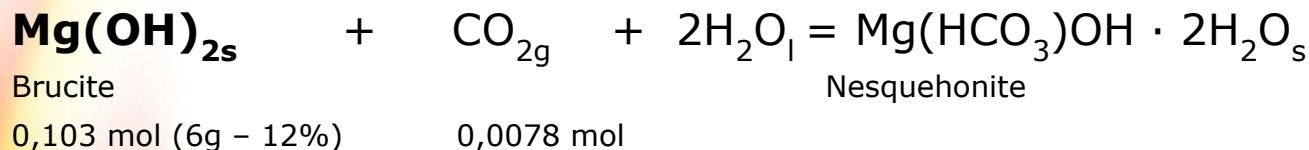
$$n(\text{CO}_2) = \frac{V(\text{CO}_2)}{V_m}$$

$$Q = -\Delta rH \cdot n$$

$$Q = Cp \cdot \Delta T$$

Chemistry of the laboratory process

50 g of ORE + 0,047 mol of CO₂ (1,06 l) :



**9 g of ore
will react
with
– 1,02 l of
 CO_2**



Carbonation reaction with Mg (OH)₂

Laboratory conditions: $\omega(\text{CO}_2) = 10\%$, $T = 298\text{K}$, 50% saturation



$$\Delta_r H = -23298 \text{ J/mol}$$

$$C_{p(\text{CO}_2)aq} = 243 \text{ J/mol}\cdot\text{K}$$

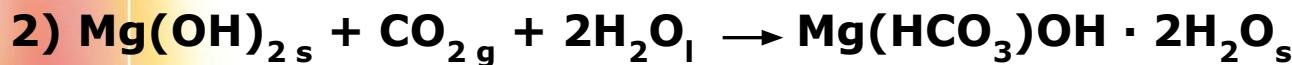
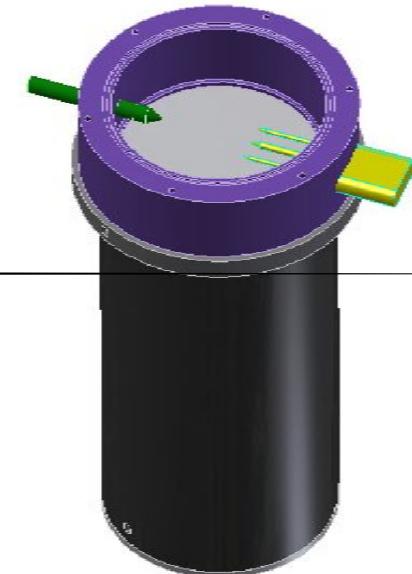
$$n(\text{CO}_2) = 0,009 \text{ mol}$$

$$Q = -\Delta_r H \cdot n = 209,68 \text{ J}$$

$$Q = C_{p(\text{CO}_2)aq} \cdot \Delta T$$

$$\Delta T = 0,86 \text{ K}$$

$$V_{\text{total}} = 2 \text{ l}$$



$$V_{\text{CO}_2} = 0,2 \text{ litres}$$

$$n(\text{CO}_2) = 0,009 \text{ mol}$$

$$\Delta_r H = -94714 \text{ J/mol of CO}_2$$

$$Q = -\Delta_r H \cdot n = 766,39 \text{ J}$$

$$Q = C_p \cdot \Delta T$$

$$\Delta T = 2,54 \text{ K}$$

Required equipment

Name	Company	Price, CAD
GMT221 Carbon Dioxide Transmitter for Incubators, Up to 20% CO₂	Vaisala	1150
pH-meter	Hanna Instruments	300
T-couple*4	Omega	150
Valves	Swagelok	380
Mg(OH)₂	Sigma Aldrich	220
SiO₂(sand)	Sigma Aldrich	215
Al₂O₃	Sigma Aldrich	150
Data acquisition card (DAQ)	National Instruments	1000
PC		?
Overall costs		~3700